

# Fundamentals of thermal convection I

Navier-Stokes-Equation (conservation of momentum)

incompressible flow

$$\rho \left( \frac{\partial \mathbf{u}}{\partial t} + \mathbf{u} \cdot \nabla \mathbf{u} \right) + \nabla p = \eta \nabla^2 \mathbf{u} + \mathbf{F}_{ext}$$

$$\nabla \cdot \mathbf{u} = 0$$

Inertial

pressure

viscous

external force

(conservation of mass)

Assumptions and approximations: incompressible flow ( $\rho = \text{const}$ ), inertial (non-rotating) frame of reference, constant Newtonian viscosity. External forces considered are gravitational forces and electromagnetic forces.

Boundary conditions:

(1)  $\mathbf{u} = 0$

impenetrable no-slip boundary

(2)  $u_n = \partial \mathbf{u}_{||} / \partial n = 0$

impenetrable free-slip boundary

Symbols (bold symbols denote vector):  $\rho$  – density,  $\mathbf{u}$  – velocity,  $p$  – pressure,  $\eta$  – dynamic viscosity,  $n$  – direction normal to boundary,  $||$  – direction parallel to boundary

# Boussinesq approximation

In thermal convection the flow is driven by differences in temperature that lead by thermal expansion to (usually small) differences in fluid density:  $\rho = \rho_o(1 - \alpha T)$ . Conflict with assumption of incompressibility. Boussinesq approximation: assume  $\rho = \text{const}$  in all terms, except in that for the external gravity force:  $\mathbf{F}_{\text{ext}} = \rho \mathbf{g} = \rho_o \mathbf{g}(1 - \alpha T)$ .  $\mathbf{g}$  given by gradient of potential: define hydrostatic pressure  $\nabla p_H = \rho_o \mathbf{g}$  and dynamic pressure  $P = p - p_H$ .

$$\frac{\partial \mathbf{u}}{\partial t} + \mathbf{u} \cdot \nabla \mathbf{u} + \nabla P / \rho_o = \nu \nabla^2 \mathbf{u} - \mathbf{g} \alpha T$$

Energy equation (heat transport equation). In the Boussinesq case, adiabatic heating and frictional heat are zero.

$$\frac{\partial T}{\partial t} + \mathbf{u} \cdot \nabla T = \kappa \nabla^2 T + H'$$

**Symbols** (index o denotes standard or reference value):  $\alpha$  – volumetric thermal expansion coefficient,  $T$  – temperature,  $\mathbf{g}$  – gravity,  $P$  – dynamic pressure,  $\nu = \eta / \rho$  – kinematic viscosity,  $\kappa$  – thermal diffusivity,  $H' = H / (\rho c_p)$  –  $H$  is specific heat generation rate per unit volume and  $c_p$  is specific heat capacity.

# Rayleigh – Bénard convection

Plane layer of height  $D$  and large (infinite) horizontal extent filled with a Newtonian fluid with constant material properties. Cartesian coordinates  $x,y,z$ ,  $\mathbf{g} = -g \mathbf{e}_z$ . Temperature fixed to  $T=T_0+\Delta T$  at  $z=0$  and  $T=T_0$  at  $z=D$ ,  $H'=0$ .

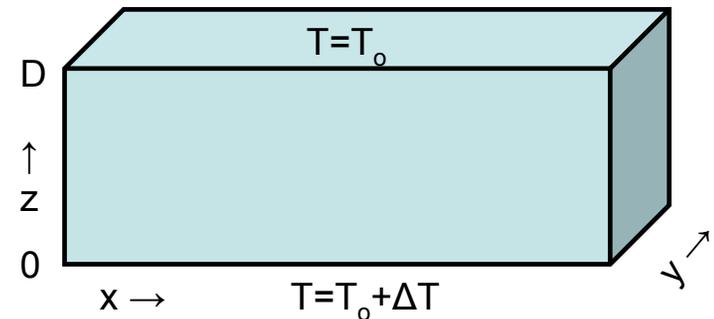
## Scaling of equations

Non-dimensional variables:  $(x',y',z') = (x,y,z)/D$ ,  $t' = t \kappa/D^2$ ,  $T'=(T-T_0)/\Delta T$ ,  $\mathbf{u}' = \mathbf{u} D/\kappa$ ,  $P' = P D^2/(\kappa\eta)$ .

Non-dimensional equations (omitting primes):

$$\frac{1}{\text{Pr}} \left( \frac{\partial \mathbf{u}}{\partial t} + \mathbf{u} \cdot \nabla \mathbf{u} \right) + \nabla P = \nabla^2 \mathbf{u} + \text{Ra} T \mathbf{e}_z$$

$$\frac{\partial T}{\partial t} + \mathbf{u} \cdot \nabla T = \nabla^2 T \quad \nabla \cdot \mathbf{u} = 0$$



$$\text{Ra} = \frac{\alpha g \Delta T D^3}{\kappa \nu} \quad \text{Pr} = \frac{\nu}{\kappa}$$

Rayleigh number                  Prandtl number

Boundary conditions:  $w = \partial u/\partial z = \partial v/\partial z = 0$  at  $z=0$  and  $z=1$ ;  $T(z=0) = 1$ ;  $T(z=1) = 0$ .

By scaling, we replace seven physical parameters ( $\alpha, \kappa, \nu, \Delta T, T_0, g, D$ ) by two numbers.

**Symbols:**  $\mathbf{e}_z$  – unit vector in  $z$ -direction (vertical),  $D$  – height of layer,  $\text{Ra}$  – Rayleigh number,  $\text{Pr}$  – Prandtl number,  $\mathbf{u} = (u,v,w)$  – cartesian velocity components

# Linear stability analysis (I)

- Trivial solution:  $T = 1 - z$ ,  $\mathbf{u} = 0$ ,  $P = 0$ . Is this solution stable, i.e. will small perturbation decay?
- In Earth's mantle  $Pr \gg 1$ , assume  $Pr = \infty$ .
- Assume 2-D solution (independence of  $y$ ,  $v=0$ ).
- Take curl of Navier-Stokes equation (eliminates pressure). Note that  $\nabla \times (T \mathbf{e}_z) = -\partial T / \partial x \mathbf{e}_y$ .
- Represent 2D incompress. flow by stream function  $\psi$ :  $\mathbf{u} = (u, 0, w) = \nabla \times (\psi \mathbf{e}_y) = (\partial \psi / \partial z, 0, -\partial \psi / \partial x)$ .
- Note that for any  $\mathbf{a}$  with  $\nabla \cdot \mathbf{a} = 0$ ,  $\nabla^2 \mathbf{a} = -\nabla \times (\nabla \times \mathbf{a})$ . Operators  $\nabla^2$  and  $\nabla \times$  commute.  $\boldsymbol{\omega} = \nabla \times \mathbf{u}$  is called vorticity.
- Perturbation  $T = 1 - z + \theta$ ,  $\theta \ll 1$ ,  $u \ll 1$ . Ignore quadratic terms in small quantities.

$$\nabla^4 \psi = Ra \frac{\partial \theta}{\partial x} \qquad \frac{\partial \theta}{\partial t} + \frac{\partial \psi}{\partial x} = \nabla^2 \theta$$

- Boundary conditions for  $\psi$  and  $\theta$ :  $\psi = \partial^2 \psi / \partial z^2 = \theta = 0$  at  $z=0$  and  $z=1$ .
- Expand into normal modes in x-direction:  $\theta = \theta_k(z, t) \exp(ikx)$ ;  $\psi = \psi_k(z, t) \exp(ikx)$ .
- Expand in harmonic function in z-direction:  $\theta_k(z, t) = \theta_{kn}(t) \sin(n\pi z)$ ,  $\psi_k(z, t) = \psi_{kn}(t) \sin(n\pi z)$ . Note that sine-functions satisfy all the boundary conditions.

**Symbols:**  $\psi$  – stream function,  $\theta$  – temperature perturbation,  $k$  – horizontal wave number

# Linear stability analysis (II)

$$(k^2+n^2\pi^2)^2 \psi_{kn} = Ra ik \theta_{kn}$$

$$d\theta_{kn}/dt = -ik \psi_{kn} - (k^2+n^2\pi^2) \theta_{kn}$$

Eliminate  $\psi_{kn}$ :

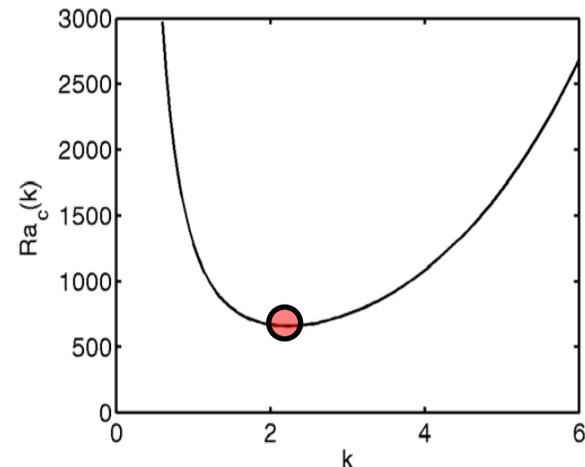
$$\frac{d\theta_{kn}}{dt} = (k^2 + n^2 \pi^2) \left( \frac{k^2 Ra}{(k^2 + n^2 \pi^2)^3} - 1 \right) \theta_{kn} = \sigma \theta_{kn}$$

The solution has the form  $\theta_{kn} \sim e^{\sigma t}$ . When, at a given value of  $Ra$ ,  $\sigma < 0$  for all  $n$  and all  $k$ , the trivial (conductive) solution is stable. When for some  $k$  and  $n$   $\sigma > 0$ , the conductive solution is unstable and convection will start. The critical Rayleigh number  $Ra_{crit}$  is found by seeking the lowest  $Ra$  for which  $\sigma=0$  is reached at any  $k, n$ . Obviously, the minimum is obtained for  $n=1$ .

$$Ra_c(k) = (k^2 + \pi^2)^3 / k^2$$

Minimum at  $k_{crit} = \pi/\sqrt{2}$ . Wavelength is  $\lambda = 2/\sqrt{2}$ .  
Width of one convection cell (aspect ratio) is  $\sqrt{2}$ .

$$Ra_{crit} = Ra_c(k_{crit}) = 27\pi^4/4 \approx 657.5$$



**Symbols:**  $\sigma$  - growth rate,  $Ra_{crit}$  - critical Rayleigh number,  $k_{crit}$  - critical wave number

# Linear stability analysis (III)

- Result unchanged when 3-D convection pattern is allowed. The critical wave number is then  $|k| = (k_x^2 + k_y^2)^{1/2} = 2\sqrt{2}$ . Linear stability cannot discriminate between different planforms of convection, which is controlled by the non-linear terms. At small super-critical Rayleigh number, the preferred pattern is two-dimensional (convection rolls).
- Result is unchanged if a finite value of Pr is retained.
- Similar analysis (although more complicated) for other boundary conditions. For example with no slip boundaries  $Ra_{\text{crit}} = 1708$ .
- In the case of internal heating,  $H > 0$ ,  $\partial T / \partial z = 0$  at  $z=0$ ,  $T=0$  at  $z=1$ , the Rayleigh number must be re-defined, replacing  $\Delta T$  by the characteristic temperature contrast in the conductive state,  $HD^2/k$

$$Ra_H = \frac{\alpha g HD^5}{k \kappa \nu}$$

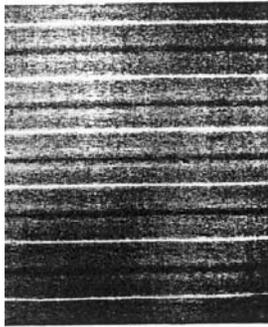
The critical Rayleigh number in this case is, with free-slip boundaries,  $Ra_{\text{crit}} = 868$ .

- In a broad range of other cases (various combinations of mechanical and thermal boundary conditions, spherical geometry) the critical Rayleigh number is typically of the order  $10^3$ .

**Symbols:**  $k_x, k_y$  – components of wavenumber vector,  $k$  – thermal conductivity,

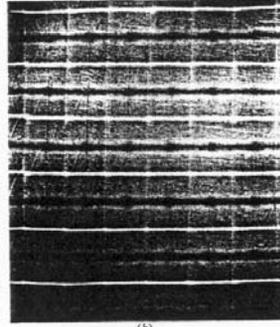
# Pattern of convection at $Ra > Ra_{crit}$

rolls



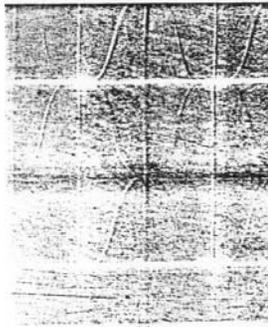
(a)

bimodal



(b)

squares



(c)

hexagons



(d)

Visualization of pattern in convection experiments by shadowgraph technique. Regular geometrical patterns are observed at moderate values of the Rayleigh number, up to  $\approx 10 Ra_{crit}$ .

At larger Rayleigh number the flow becomes irregular and time-dependent.

**Symbols:**  $k_x, k_y$  – components of wavenumber vector,  $k$  – thermal conductivity,

# Application to Earth and Planets

For Earth's mantle select characteristic values:

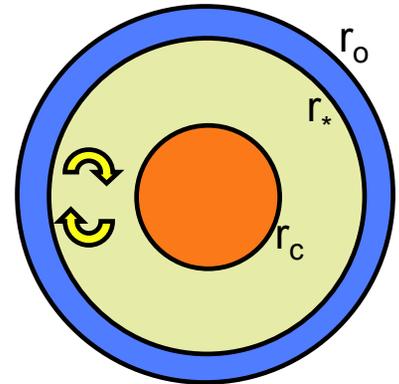
$$\alpha = 2 \times 10^{-5} \text{ K}^{-1} \quad \Delta T = 2000 \text{ K} \quad g = 10 \text{ m/s}^2 \quad D = 2,900,000 \text{ m}$$

$$\kappa = 10^{-6} \text{ m}^2/\text{s} \quad \rho = 4000 \text{ kg/m}^3 \quad \eta = 10^{21} - 10^{22} \text{ Pa s} \quad (\text{from postglacial rebound})$$

$$\Rightarrow \quad Ra = 4 \times 10^6 \quad \dots \quad 4 \times 10^7 \quad \gg \quad Ra_{\text{crit}}$$

For other planets, assume similar values for  $\alpha$ ,  $\rho$ ,  $\kappa$ ,  $\eta$ . Use  $Ra_H$  with the „chondritic“ value of radiogenic heating  $H = 1.6 \times 10^{-8} \text{ Wm}^{-3}$  ( $H' = 4 \times 10^{-15} \text{ K/s}$ ). Without plate tectonics convection takes place below a rigid outer shell whose bottom at radius  $r_*$  is given by a temperature of  $T_* \approx 1300 \text{ K}$  (heat is conducted in the shell). In a conducting, internally heated sphere  $T(r) = H'/(6\kappa) [r_o^2 - r^2] + T_o \Rightarrow r_*^2 = r_o^2 - 6\kappa(T_* - T_o)/H'$ . Set  $D = r_* - r_c$ .

	$r_o$ [km]	$r_c$ [km]	$T_o$ [K]	$r_*$ [km]	$g_o$ [m/s <sup>2</sup> ]	$Ra_H$
Venus	6050	3200	720	5950	8.9	$4 \times 10^8$
Mars	3400	1500	220	3060	3.7	$1 \times 10^7$
Moon	1740	400	250	960	1.6	$3 \times 10^4$



**Symbols:**  $r_o$  – outer radius of planet,  $T_o$  – temperature at  $r_o$ ,  $T_*$  - transitional temperature,  $r_*$  - radius of lithosphere-asthenosphere boundary,  $r_c$  – core radius,  $g_o$  – gravity at surface